Table 1 – Physico-chemical characteristics of Ni / Al-HMS-bentonite catalysts with a Si/Al ratio = 20

| Catalyst | SSA, m ² /g | D _{pores} , nm | Ti V |
|-------------------------|------------------------|-------------------------|---|
| Ni/Al-HMS(20)-bentonite | 570 | 4,1 | v _{pores} , cm ³ /g |
| | | | 0,8 |

As follows from the data of Figure 1, the nitrogen adsorption/desorption isotherm for the Ni/Al-HMS (20)-bentonite sample is characterized by a slightly wide hysteresis loop. Nickel promotion of catalysts based on mesoporous aluminosilicate leads to significant changes in the structural characteristics of the catalyst compared to the nitrogen adsorption/desorption isotherm for the Al-HMS (20) sample [20]. There are three peaks observed on the pore effective diameters distribution curve: one of which corresponds to the mesoporous aluminosilicate, the second - to bentonite and the third - to the promoting additive. The sample under study is characterized by a high specific surface area, which is of 570 m²/g.

Hexadecane was used in order to establish the mechanism of heavy petroleum residues hydroisomerization in the presence of a composite based on the mesoporous aluminosilicate and bentonite, promoted by nickel.

Process of hexadecane transformation on the compositeon a basis of the promoted mesoporous aluminosilicatewas studied in a temperature interval of 300-450 °C, at a feed rates – 1 h⁻¹, under hydrogen pressure and at a hydrogen/raw materials ratio of 100 (vol.). The experimental data are provided in tables 2, 3.

 $\label{eq:table 2-The action of the temperature on the group hydrocarbon-type content} for the products of hexadecane transformation on the Ni/Al-HMS(20)-bentonite composite, Wfeed rate = 1,0 h^-l, P_{H2}= 3 MPa$

| № Hydrocarbon-type co | II. I salvan tema content | Content by mass % | | | |
|-----------------------|---------------------------|-------------------|--------|--------|--|
| | Hydrocarbon-type content | 300 °C | 350 °C | 450 °C | |
| 1 | N-paraffins | 31,98 | 36,39 | 43,02 | |
| 2 | Isoparaffins | 45,23 | 39,76 | 12,41 | |
| 3 | Arenes | 5,20 | 8,25 | 7,16 | |
| 4 | Naphthenes | 8,66 | 8,41 | 15,83 | |
| 5 | Olefins | 5,23 | 4,10 | 14,98 | |
| 6 | Dienes | 0,70 | 0,80 | 5,30 | |
| 7 | Cycloolefins | 2,25 | 2,04 | 0,67 | |
| 8 | Cyclodienes | 0,75 | 0,25 | _ | |

From the experimantal data obtained (table 2) it is seen that isomerization process is the main direction of hexadecane transformation under the conditions of low-temperature alumiosilicate catalysis (300 °C). It also should be noted that isometric structures of hexadecane are obtained due to isomerization process, without cracking participation. As the temperature rises from 300 to 350 °C